WHAT IS CLAIMED IS:

1. A process for producing a xylylenediamine by hydrogenating a dicyanobenzene in a liquid phase in the presence of a catalyst, the process comprising a step of bringing the catalyst having its activity decreased during the course of the hydrogenation of dicyanobenzene into contact with a hydrogen-containing gas at 200 to 500°C while controlling a temperature rise speed of the catalyst to 40°C/min or less, thereby regenerating the catalyst; and a step of reusing the catalyst thus regenerated in the subsequent hydrogenation of the dicyanobenzene.

2. The process according to Claim 1, wherein a feed rate of hydrogen is regulated so as to control a temperature rise speed of the catalyst to 40°C/min or less during under contact with the hydrogen-containing gas.

3. The process according to Claim 1, wherein the step for regenerating the catalyst comprises the following treatments (1) and (2):

(1) bringing the catalyst into contact with a hydrogen-containing gas at 140 to 200°C for one hour or longer while controlling an average treating temperature to 180°C or lower, and then

(2) further bringing the catalyst thus treated into contact with a hydrogen-containing gas at 200 to 500°C.

4. The process according to Claim 1, wherein the hydrogenation of dicyanobenzene is conducted in a fixed bed reactor.

5. The process according to Claim 1, wherein the catalyst is a nickel- and/or cobalt-containing catalyst.

6. The process according to Claim 1, wherein the catalyst is a nickel-containing catalyst.

7. A process for producing a xylylenediamine by hydrogenating a dicyanobenzene in a liquid phase in the presence of a catalyst, the process comprising a step of regenerating the catalyst having its activity decreased during the course of the hydrogenation of the dicyanobenzene by the following

treatments (1) and (2):

(1) bringing the catalyst into contact with a hydrogen-containing gas at 140 to 200°C for one hour or longer while controlling an average treating temperature to 180°C or lower, and then

(2) further bringing the catalyst thus treated into contact with a hydrogen-containing gas at 200 to 500°C; and

a step of reusing the catalyst thus regenerated in the subsequent hydrogenation of the dicyanobenzene.

8. The process according to Claim 7, wherein the step (1) is performed while controlling a temperature rise speed of the catalyst to 40°C/min or less.

9. The process according to Claim 8, wherein the step (1) is performed while regulating a feed rate of the hydrogen-containing gas so as to control the temperature rise speed of the catalyst to 40°C/min or less.

10. The process according to Claim 9, wherein the step (1) is performed by feeding the hydrogen-containing gas at a rate of 0.001 to 1000 L/h on a basis of a normal state of 0°C and 1 atm per 1 kg of the catalyst.

11. The process according to Claim 7, wherein the steps (1) and (2) are performed while controlling a temperature rise speed of the catalyst to 40°C/min or less.

12. The process according to Claim 11, wherein the steps (1) and (2) are performed while regulating a feed rate of the hydrogen-containing gas so as to control the temperature rise speed of the catalyst to 40°C/min or less.

13. The process according to Claim 12, wherein the steps (1) and (2) are performed by feeding the hydrogen-containing gas at a rate of 0.001 to 1000 L/h on a basis of a normal state of 0°C and 1 atm per 1 kg of the catalyst.

14. The process according to Claim 7, wherein the hydrogenation of dicyanobenzene is conducted in a fixed bed reactor.

15. The process according to Claim 7, wherein the catalyst is a nickel- and/or cobalt-containing catalyst.

16. The process according to Claim 7, wherein the catalyst is a nickel-containing catalyst.